

# **Centrex Technical Sales**

#### 804-354-1511

### **Pump Inquiry Application Data Sheet**

The following information is required to prope	erly process ar	n inquiry:	
Requested by	Date		
Customer			
Address			
TelephoneFax		Email	
Description of product to be pumped			
Femperature Specific Gravity	or D	ensity	lb./gal
/iscosity	Centipoi	se (CPS) or other	
Desired Flow Rate			
Discharge Head			
Suction Conditions:			
Is the pump withdrawing from a vacuum?	Yes	No	
If so, how much?in. Hg.			
s the product level on the inlet side of the pun	np above or be	low the center line of the	pump inlet?
AboveBelowBy how			
Tubing in. DiameterLength			No. of tees
Tubing in. DiameterLength		No. of elbows	No. of tees
No. of size of valves in suction piping:			
No	Size (in.)		
No			
Other equipment in the suction piping			
If you do not know the desired discharge head	d, please provi	de the following:	
<b>Discharge Conditions</b> s the final destination of the pump above or be	alow the cente	or line of the numn inlet?	
AboveBelowBy h			
Tubingin. Diameter Len			No of tees
Tubingin. Diameter Len			
Tubingin. Diameter Len	oth	No. of elbows	No. of tees
No. and size of valves in discharge piping:	Bui		110.01 100
NoNo	size (in )		
No			
No.		*	
Other equipment and the drop or pressure req		in the dischause wining	

#### **How To Calculate Required Pressure**

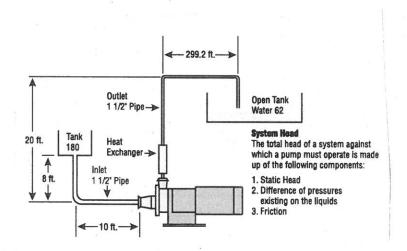
#### **Example:**

Find the head under these conditions: Pump is drawing from an open tank to discharge through a heat exchanger into an open tank that is 20 ft. above the pump. The supply is 8 ft. above the pump. 50 GPM flow is required.

#### Solution:

1. Height to be pumped is 20 ft. minus 8 ft.	=12.0 ft.
2. Friction loss from pipe is	
(8 ft. + 10 ft. + 20 ft. + 299.2 ft. = 337.2 ft.) 337.2 x .25 ft./ft.	=84.3 ft.
3. Friction loss from 3 elbows is = 0.6 ft.	= 0.6  ft.
4. *Heat Exchanger loss 2.31 times 16.5 PSI	=38.1 ft.
The Total Head Loss is	135.0 ft.

<sup>\*</sup>Heat Exchanger information supplied by manufacturer.



#### **Determining Net Positive Suction Head (NPSH)**

Due to the hydraulic principles involved, some level of NPSH is required in order for the pump to run efficiently and without cavitating. The NPSH required for each sanitary centrifugal pump model has been determined by careful testing. The results of these tests are illustrated by the NPSH requirement shown on the pump curve.

To determine the NPSH available, first add the physical height of the liquid above the centerline of the pump inlet to the pressure above the liquid (in an open tank this is atmospheric pressure). From this total, subtract the friction losses of the line and fittings on the suction side and the vapor pressure of the liquid at the operating temperature. The remainder is the NPSH available. This number must meet or exceed the NPSH required in order for the pump to function properly.

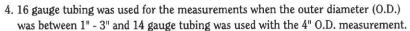
# Loss of Head Due to Friction in Feet per Foot of Stainless Steel Tubing and in Feet for Sanitary Fittings

Notes:

1. Flow Elbows—R/D = 1.5

2. Flow Through Tees—Flow A to B Port C capped off.

3. Test Medium-Water at 70°F



<sup>\*</sup>Calculated data for estimating purposes only. Consult your tubing manufacturer with specific questions.

В

Capacity in	O.D			10/1/2015	- 1.5"		O.D			0.D.			0.D			O.D		
U.S. G.P.M.	I.D				- 1.370	1	I.D			I.D.		)"	I.D		n	I.D		0
	Tubing	Elbow	Tee	Tubing	Elbow	Tee	Tubing	Elbow	Tee	Tubing	Elbow	Tee	Tubing	Elbow	Tee	Tubing	Elbow	Tee
2	.01	.01	.1															
4	.025	.02	.2															
5	.035	.025	.25				540											
10	.12	.06	.4	.02	.01	.15	.005	.015	.1									
15	.25	.1	.8	.04	.02	.25	.013	.02	.15									
20	.43	.22	1.5	.06	.03	.3	.02	.025	.2	.005	.02	.1	.003	.02	.06			
25	.66	.4	2.3	.08	.04	.4	.025	.03	.25	.006	.03	.15	.004	.03	.08			
30	.93	.7	3.3	.105	.06	.55	.035	.05	.3	.008	.05	.2	.005	.04	.1			
35	1.22	1.25	5.2	.135	.09	.8	.04	.06	.4	.011	.06	.25	.006	.05	.13			
40				.17	.11	1.0	.05	.08	.5	.015	.07	.3	.007	.06	.15			
45				.21	.16	1.3	.063	.1	.6	.02	.09	.35	.008	.065	.18			
50				.25	.2	1.6	.073	.12	.7	.022	1	.4	.01	.07	.2			
60				.34	.35	2.2	.1	.18	.9	.03	.12	.45	.015	.08	.25			
80				.57	.76	3.7	.16	.3	1.5	.05	.15	.55	.02	.1	.4			
100				.85	1.35	5.8	.23	.44	2.3	.075	.18	.6	.03	.11	.5	.008	.04	.1
120				1.18	2.05	9.1	.32	.64	3.3	.105	.21	1.0	.04	.13	.6	.01	.05	.15
140							.42	.85	4.5	.14	.23	1.25	.05	.16	.8	.013	.06	.2
160							.54	1.13	5.8	.17	.28	1.6	.07	.2	1.1	.015	.07	.25
180							.67	1.45	7.4	.205	.31	2.0	.08	.21	1.3	.02	.08	.3
200	= 0						.81	1.82	9.0	.245	.35	2.5	.1	.26	1.6	.025	.09	.4
220							.95	2.22	11.0	.29	.41	3.0	.12	.3	1.9	.028	.1	.5
240							1.10	2.63	13.5	.34	.48	3.7	.14	.33	2.2	.035	.11	.55
260										.39	.53	4.5	.165	.39	2.5	.04	.115	.6
280										.45	.61	5.3	.19	.42	2.8	.045	.12	.65
300										.515	.7	6.2	.22	.5	3.1	.05	.13	.7
350										.68	1.05	8.5	.28	.67	4.1	.07	.15	.9
400										.86	1.55	11.0	.36	.88	5.2	.085	.18	1.2
450										1.05	2.25	13.5	.44	1.1	6.6	.105	.2	1.5
500	-												.54	1.4	8.0	.13	.23	1.75
550										2 37 37 33			.64	1.7	9.5	.15	.27	2.1
600						1.5				1			.75	2.05	10.2	1.175	.3	2.5
650													.87	2.41	13.0	.2	.34	2.8
700					1								1.0	2.8	15.0	.23	.4	3.4
750																.26	.43	3.8
800																.3	.5	4.4
850			- 33 AA-81-0													.33	.56	5.0
900																.37	.62	5.7
950					7755											.41	.7	6.3
1000														NAME OF THE OWNER.		.45	.8	7.0
1100																.53	1.06	8.6

## **Conversion Factors**

Length			
Meters	X	3.281	= Feet
Centimeters	Х	0.394	= Inches
Millimeters	X	0.0394	= Inches
Mass			
Kilograms	Χ	2.2	= Lbs.
Gallons Of Water	X	8.34	= Lbs.
Cubic Feet of Water	X	62.4	= Lbs.
Pounds	X	0.454	= Kilograms
Volume			
Liter	X	0.264	= Gallon
Cubic Feet	X	7.48	= Gallon
Lbs. Of Water	X	0.119	= Gallon
Imperial Gallon			
(British)	X	1.2	= Gallon (U.S.)
U.S. Gallon	X	3.785	= Liter
Pressure			
Feet of Water	X	0.433	= PSI
Inches of Hg.	Х	0.491	= PSI
Atmosphere	Х	14.7	= PSI
Meters of Water	X	1.42	= PSI
Kilograms/sq.			
Centimeter	X	14.22	= PSI
Bar	X	14.7	= PSI

ied)		
X	33.9	= Feet of Water
X	2.31	= Feet of Water
X	1.13	= Feet of Water
X	0.002	= GPM
X	0.002	= GPM
X	4.4	= GPM
X	0.264	= GPM
X	0.264	= GPM
X	3.785	= Liters/Minute
3 ead f	960 t. x Speci	fic Gravity
A I U	mp Emon	onoy
= 0	entistoke	es
X	4.64	= SSU (Approx.
	x x x x x x x x x x x x x x = ead ff x Pu	x 33.9 x 2.31 x 1.13 x 0.002 x 0.002 x 4.4 x 0.264 x 0.264 x 3.785 ead ft, x Speci x Pump Efficion

(1.8 X °C) + 32 = °F .555 (°F - 32°) = °C Degrees Kelvin - 273.2 = Degrees Centigrade

# **Vapor Pressure Chart**



